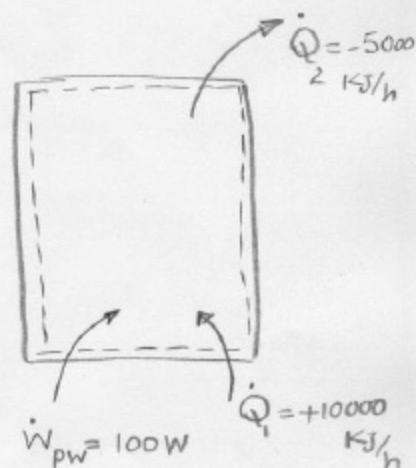
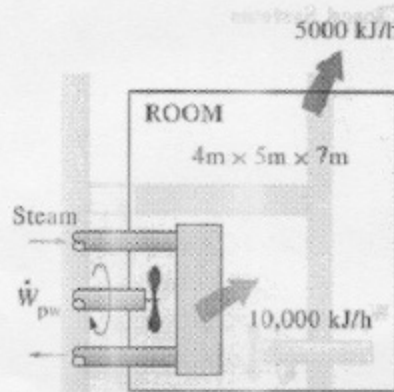


**Introduction to Thermodynamics and Heat Transfer (ECE 309)**  
Suggested Problems for Chapter 3

1. A  $4\text{ m} \times 5\text{ m} \times 7\text{ m}$  room is heated by the radiator of a steam-heating system as shown in Fig. 1. The steam radiator transfers heat at a rate of  $10,000\text{ kJ/h}$ , and a  $100\text{ W}$  fan is used to distribute the warm air in the room. The rate of heat loss from the room is estimated to be about  $5000\text{ kJ/h}$ . If the initial temperature of the room air is  $10^\circ\text{C}$ , determine how long it will take for the air temperature to rise to  $20^\circ\text{C}$ . Assume constant specific heats at room temperature.



$$T_i = 10^\circ\text{C}$$

$$\Delta t = ? \text{ for } T = 20^\circ\text{C}$$

$$\dot{Q}_{\text{net}} - \dot{W}_{\text{net}} = \frac{dE}{dt} = \frac{dU}{dt} \quad \text{or} \quad (\dot{Q}_{\text{net}} - \dot{W}_{\text{net}}) \Delta t = \Delta U$$

$$dU = m c_v dT \quad \text{or} \quad \Delta U = m c_v \Delta T$$

$$m = \frac{PV}{RT_i} = \frac{(100\text{ kPa})(4 \times 5 \times 7)\text{ m}^3}{(0.287\text{ kPa m}^3)(10 + 273)\text{ K}} = 172.4\text{ kg}$$

$$c_v = 0.718\text{ kJ/kg}^\circ\text{C} \quad (\text{Table A-2a})$$

$$\therefore [(10000 - 5000)/3600 - (-1)] \Delta t = 172.4 \times 0.718 \times (20 - 10)$$

$$\Rightarrow \boxed{\Delta t = 831.4\text{ Sec}}$$

2. A piston-cylinder device contains 0.8 kg of nitrogen initially at 100 kPa and 27 °C. The nitrogen is now compressed slowly in a polytropic process during which  $PV^{1.3} = C$  until the volume is reduced by one-half. Determine the work done and the heat transfer for this process.

$$m = 0.8 \text{ kg}$$

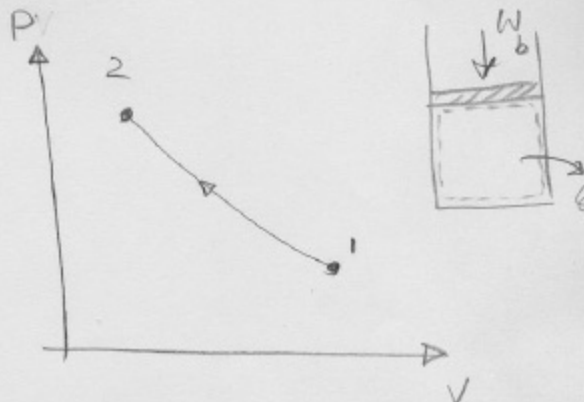
$$P_1 = 100 \text{ kPa}$$

$$T_1 = 27^\circ \text{C}$$

$$PV^{1.3} = C$$

$$V_2 = \frac{1}{2} V_1$$

$$\begin{cases} W = ? \\ Q = ? \end{cases}$$



$$W_b = \int_1^2 P dV = \dots = \frac{P_2 V_2 - P_1 V_1}{1-n} = \frac{m R (T_2 - T_1)}{1-n}$$

$$P_1 V_1^{1.3} = P_2 V_2^{1.3} = C \Rightarrow P_2 = P_1 \left( \frac{V_1}{V_2} \right)^{1.3} = 100 \left( \frac{2}{1} \right)^{1.3} = 246.2 \text{ kPa}$$

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2} \Rightarrow T_2 = T_1 \left( \frac{P_2 V_2}{P_1 V_1} \right) = (27 + 273) \left[ \frac{246.2 \times 1}{100 \times 2} \right]$$

$$T_2 = 369.3 \text{ K} = 96.3^\circ \text{C} \leftarrow$$

$$W_b = \frac{0.8 \text{ kg} \times 2968 \frac{\text{kJ}}{\text{kg K}} \times (96.3 - 27) \text{ K}}{1 - 1.3} = -54.8 \text{ kJ} \leftarrow$$

$$\boxed{W_b = -54.8 \text{ kJ}}$$

$$Q - (W_b + W_{\text{other}}) = \Delta U$$

$$\begin{aligned} Q = \Delta U + W_b &= m C_v^* (T_2 - T_1) + W_b \\ &= 0.8 \times 1.744 (96.3 - 27) - 54.8 \end{aligned}$$

$$\boxed{Q = -13.55 \text{ kJ}} \leftarrow$$

3. A rigid tank containing  $0.4 \text{ m}^3$  of air at  $400 \text{ kPa}$  and  $30^\circ\text{C}$  is connected by a valve to a piston-cylinder device with zero clearance (Fig. 2). The mass of the piston is such that a pressure of  $200 \text{ kPa}$  is required to raise the piston. The valve is now opened slightly, and air is allowed to flow into the cylinder until the pressure in the tank drops to  $200 \text{ kPa}$ . During this process, heat is exchanged with the surroundings such that the entire air remains at  $30^\circ\text{C}$  at all times. Determine the heat transfer for this process.

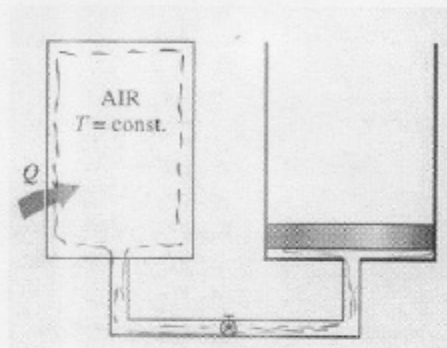


Fig. 2

$$P_1 = 400 \text{ kPa}, \quad T_1 = 30^\circ\text{C}, \quad V_1 = 0.4 \text{ m}^3$$

$$P_2 = 200 \text{ kPa}, \quad T_2 = T_1 = 30^\circ\text{C}$$

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2} \quad \text{or} \quad P_1 V_1 = P_2 V_2 \quad \text{or} \quad PV = cTe \quad \text{or} \quad P = \frac{c}{V}$$

$$V_2 = \left(\frac{P_1}{P_2}\right) V_1 = \left(\frac{400}{200}\right) \times 0.4 = 0.8 \text{ m}^3 \leftarrow$$

$$W_b = \int_1^2 P dV = c \ln \frac{V_2}{V_1} = P_1 V_1 \ln \frac{V_2}{V_1} = (400 \times 0.4) \ln \frac{0.8}{0.4}$$

$$W_b = 110.9 \text{ kJ}$$

$$Q - (W_b + W_{\text{other}}) = \Delta U \quad \text{since } \Delta T = 0$$

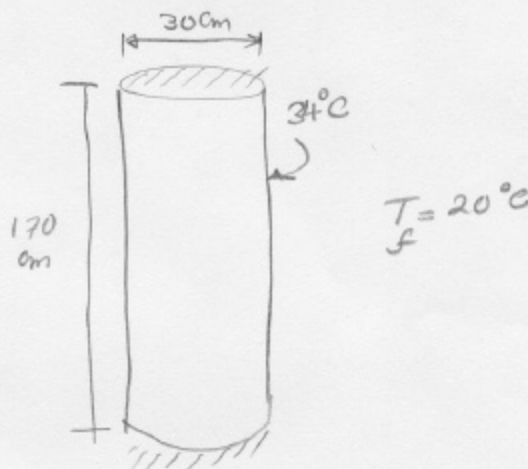
$$Q = W_b = 110.9 \text{ kJ}$$

4. It is well known that wind makes cold air feel much colder as a result of the wind-chill effect, which is due to the increase in the convection heat transfer coefficient as a result of the increase in air velocity. The wind-chill effect is usually expressed in terms of the wind-chill factor, which is the difference between the actual air temperature and the equivalent calm-air temperature. For example, a wind-chill factor of  $20^\circ\text{C}$  for an actual air temperature of  $5^\circ\text{C}$  means that the windy air at  $5^\circ\text{C}$  feels as cold as the still air at  $-15^\circ\text{C}$ . In other words, a person will lose as much heat to air at  $5^\circ\text{C}$  with a wind-chill factor of  $20^\circ\text{C}$  as he or she would in calm air at  $-15^\circ\text{C}$ .

For heat transfer purposes, a standing naked man can be modeled as a 30-cm-diameter, 170-cm-long vertical cylinder with both the top and bottom surfaces insulated and with the side surface at an average temperature of  $34^\circ\text{C}$ . For a convection heat transfer coefficient of  $15\text{ W}/(\text{m}^2\cdot^\circ\text{C})$ , determine the rate of heat loss from this man by convection in still air at  $20^\circ\text{C}$ . What would your answer be if the convection heat transfer coefficient was increased to  $50\text{ W}/(\text{m}^2\cdot^\circ\text{C})$  as a result of winds? What is the wind-chill factor in this case?

$$h_1 = 15\text{ W}/(\text{m}^2\cdot^\circ\text{C})$$

$$\dot{Q} = ?$$



$$(a) \quad \dot{Q}_1 = h A (T_s - T_f) = 15 \times (\pi \times 0.3 \times 1.7) (34 - 20)$$

$$\dot{Q}_1 = 336.5\text{ W}$$

(b) for windy condition

$$\dot{Q}_2 = h A (T_s - T_f) = 50 \times (\pi \times 0.3 \times 1.7) \times (34 - 20) = 1121.55\text{ (W)}$$

$$(c) \quad 1121.5 = 15 \times (\pi \times 0.3 \times 1.7) (34 - T_{\text{eff}})$$

$$T_{\text{eff}} = -12.7^\circ\text{C}$$

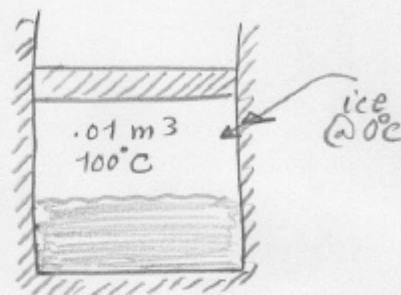
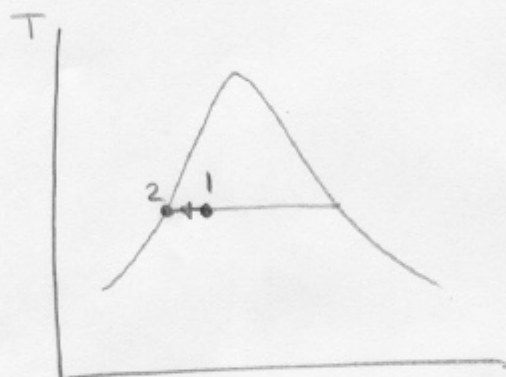
$$\text{ON Windchill factor} = 20 - (-12.7) = 32.7^\circ\text{C} \quad \leftarrow$$

5. An insulated piston-cylinder device initially contains  $0.01 \text{ m}^3$  of saturated liquid-vapor mixture with a quality of 0.2 at  $100^\circ\text{C}$ . Now some ice at  $0^\circ\text{C}$  is added into the cylinder. If the cylinder contains saturated liquid at  $100^\circ\text{C}$  when thermal equilibrium is established, determine the amount of ice added. The melting temperature and the heat of fusion of ice at atmospheric pressure are  $0^\circ\text{C}$  and  $333.7 \text{ kJ/(kg}\cdot^\circ\text{C)}$ , respectively.

$$V_1 = 0.01 \text{ m}^3$$

$$x_1 = 0.2$$

$$T = 100^\circ\text{C}$$



$$v_f = 0.001044 \text{ (m}^3/\text{kg)}$$

$$v_g = 1.6729 \text{ (m}^3/\text{kg)}$$

$$h_f = 419.04 \text{ (kJ/kg)}$$

$$h_g = 2676.1 \text{ (kJ/kg)}$$

$$v_1 = v_f + x v_{fg} = 0.001044 + 0.2(1.6729 - 0.001044) = 0.3354 \text{ m}^3/\text{kg}$$

$$h_1 = h_f + x h_{fg} = 419.04 + 0.2(2676.1 - 419.04) = 870.4 \text{ kJ/kg}$$

$$h_2 = h_f = 419.04$$

$$m_1 = \frac{V_1}{v_1} = \frac{0.01}{0.3354} = 0.0298 \text{ kg}$$

$$\Delta h = (870.4 - 419.04) = 451.36 \text{ kJ/kg}$$

$$\text{or } \Delta H = 451.36 \times 0.0298 = 13.45 \text{ kJ}$$

$$\Delta H = m_{ice} c_{ice} (\Delta T)_{ice} + m_{ice} h_{fus}$$

$$= m_{ice} [c_{ice} \Delta T + h_{fus}]$$

$$13.45 = m_{ice} [4.184 \times 100 + 333.7]$$

$$m_{ice} = 0.0179 \text{ kg or } 17.9 \text{ kg}$$

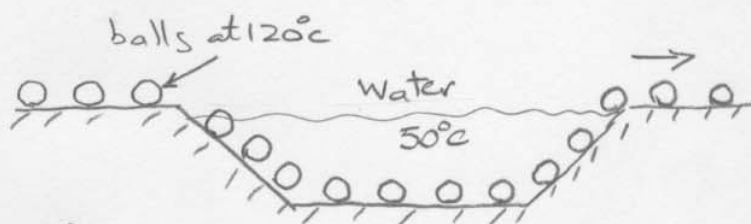
ch. 3Problem 6Assumptions

- Thermal properties of the balls are constant
- balls are at a uniform temp before and after quenching

$$- \Delta KE = \Delta PE \approx 0$$

$$\rho_{Al} = 2700 \text{ (kg/m}^3\text{)}$$

$$C_{pAl} = 0.959 \text{ (kJ/kg}\cdot\text{C)}$$

Solution

We take a single ball as the system. The energy balance for this closed system is,

$$\underbrace{E_{in} - E_{out}}_{\substack{\text{net energy transfer} \\ \text{by heat, work, and mass}}} = \underbrace{\Delta E_{system}}_{\substack{\text{changes in internal, kinetic,} \\ \text{potential, etc.}}}$$

$$-Q_{out} = \Delta U_{ball} = m(u_2 - u_1)$$

$$Q_{out} = mc(T_1 - T_2)$$

the total amount of heat transfer from a ball is;

$$m = \rho V = \rho \frac{\pi D^3}{6} = 2700 \text{ (kg/m}^3\text{)} \frac{\pi (0.05 \text{ m})^3}{6} = 0.1767 \text{ (kg)}$$

$$Q_{out} = mc(T_1 - T_2) = 0.1767 \text{ (kg)} \cdot 0.959 \text{ (kJ/kg}\cdot\text{C)} (120 - 74) \\ = 7.80 \text{ (kJ/ball)}$$



Then the rate of heat transfer from the balls to the water becomes

$$\dot{Q}_{\text{total}} = \dot{n}_{\text{ball}} \dot{Q}_{\text{ball}} = 100 \frac{\text{ball}}{\text{min}} \times 7.80 \frac{\text{kJ}}{\text{ball}}$$

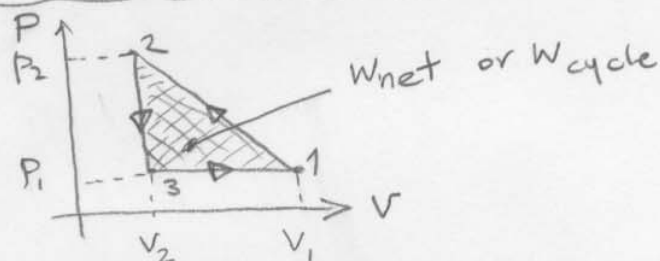
$$= 780 \frac{\text{kJ}}{\text{min}}$$

Therefore, heat must be removed from the water at a rate of  $780 \text{ kJ/min}$  in order to keep its temp constant at  $50^\circ\text{C}$ .

Since energy input must be equal to energy output for a system whose energy level remains constant.

$$E_{\text{in}} = E_{\text{out}} \quad \text{when} \quad \Delta E_{\text{system}} = 0$$

Problem 7



$$W_{\text{cycle}} = W_{12} + W_{23} + W_{31}$$

$$\left\{ \begin{aligned} W_{12} &= - \int_1^2 p \, dv = - \left( \frac{P_1 + P_2}{2} \right) (V_2 - V_1) = - \left( \frac{P_1 + P_2}{2} \right) (V_1 - V_2) \end{aligned} \right.$$

$$\left\{ \begin{aligned} W_{23} &= - \int_2^3 p \, dv = 0 \quad \text{Since } dv = 0 \end{aligned} \right.$$

$$\left\{ \begin{aligned} W_{31} &= - \int_3^1 p \, dv = -P_1 (V_1 - V_3) = -P_1 (V_1 - V_2) \end{aligned} \right.$$

$$W_{\text{cycle}} = \left( \frac{P_1 + P_2}{2} \right) (V_1 - V_2) - P_1 (V_1 - V_2)$$

Note that is equal to the cross-hatched area in the p-v diagram. Also, in such a cyclic process,

$$\Delta U = \Delta T = \Delta P = \Delta(\text{any property}) = 0$$