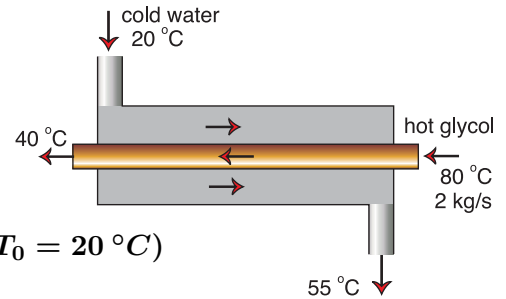


ME354
Thermodynamics 2

Quiz #2 - T02:

Name: _____
ID #: _____

Problem: An adiabatic heat exchanger is to cool ethylene glycol ($c_p = 2.56 \text{ kJ/kg} \cdot ^\circ\text{C}$) flowing at a rate of 2 kg/s from 80 to 40 $^\circ\text{C}$ by water ($c_p = 4.18 \text{ kJ/kg} \cdot ^\circ\text{C}$) that enters at 20 $^\circ\text{C}$ and leaves at 55 $^\circ\text{C}$. Determine:



- (a) the rate of heat transfer [kW] and
- (b) the rate of exergy destruction [kW] in the heat exchanger ($T_0 = 20$ $^\circ\text{C}$)

Assumptions

1. SS-SF
2. heat loss to the surroundings is negligible
3. $KE = PE \rightarrow 0$
4. properties are constant

Part a)

The rate of heat transfer can be determined from a heat balance between the two flow streams.

$$\begin{aligned} \dot{E}_{in} &= \dot{E}_{out} \\ \dot{m}h_{in} &= \dot{Q}_{out} + \dot{m}h_{out} && \text{1 mark} \\ \dot{Q}_{out} &= \dot{m}c_p(T_{in} - T_{out}) \quad (\text{since } KE=PE=0) \end{aligned}$$

The rate of heat transfer out of the glycol is

$$\dot{Q}_{out} = [\dot{m}c_p(T_{in} - T_{out})]_{glycol} = (2 \text{ kg/s})(2.56 \text{ kJ/kg} \cdot ^\circ\text{C})(80 - 40) ^\circ\text{C} = 204.8 \text{ kW} \leftarrow$$

2 marks

Part b)

Applying the second law to the entire heat exchanger we get

$$\begin{aligned} \dot{S}_{in} - \dot{S}_{out} + \dot{S}_{gen} &= \Delta \dot{S}_{system} \stackrel{0}{=} \text{(SS)} \\ \dot{m}_{glycol}s_1 + \dot{m}_{water}s_3 - \dot{m}_{glycol}s_2 + \dot{m}_{water}s_4 + \dot{S}_{gen} &= 0 && \text{1 mark} \\ \dot{m}_{glycol}(s_2 - s_1) + \dot{m}_{water}(s_4 - s_3) &= \dot{S}_{gen} \end{aligned}$$

The mass flow rate of the water can be determined by noting that $\dot{Q}_{out,glycol} = \dot{Q}_{in,water}$, therefore

$$\dot{m}_{water} = \frac{\dot{Q}_{in,water}}{c_p(T_{out} - T_{in})} = \frac{204.8 \text{ kJ/s}}{(4.18 \text{ kJ/kg} \cdot ^\circ\text{C})(55 - 20) ^\circ\text{C}} = 1.4 \text{ kg/s} \quad \text{2 marks}$$

For an incompressible substance

$$\Delta s = c_p \ln \frac{T_2}{T_1} \quad \boxed{1 \text{ mark}}$$

Therefore

$$\begin{aligned} \dot{S}_{gen} &= \dot{m}_{glycol} c_p \ln \frac{T_2}{T_1} + \dot{m}_{water} c_p \ln \frac{T_4}{T_3} \\ &= (2 \text{ kg/s}) \left(2.56 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right) \ln \frac{40 + 273.15}{80 + 273.15} + (1.4 \text{ kg/s}) \left(4.18 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right) \ln \frac{55 + 273.15}{20 + 273.15} \\ &= 0.045 \text{ kW/K} \quad \boxed{2 \text{ marks}} \end{aligned}$$

The exergy destroyed is found as

$$\dot{X}_{des} = T_0 \dot{S}_{gen} = (293.15 \text{ K})(0.045 \text{ kW/K}) = 13.1 \text{ kW} \quad \boxed{1 \text{ mark}}$$