## Week 3

## Lecture 1

ME 353 Web Site: Summary of week 2 topics are on the Web. Contact resistance:  $R_c = 1/(h_c A)$ ; see Table 3.1 for typical values of  $R''_{t,c}$ ; how to get  $h_c$ , contact conductance, from Table 3.1;  $h_c = 1/R''_{t,c} [W/m^2 K]$ . Thermal resistance R of composite systems.

Overall conductance U for cylindrical systems. This parameter has units of  $[W/m^2 \cdot K]$ .

Definitions of  $U_i$  and  $U_o$  and relationships.

$$Q_{sys} = U_i A_i (T_{f1} - T_{f2}) = U_o A_o (T_{f1} - T_{f2}) = (T_{f1} - T_{f2}) / R_{total}$$

where  $A_i$  and  $A_o$  are the inner and outer surface areas and  $A_o > A_i$ . Since  $U_i A_i = U_o A_o$ , then  $U_i > U_o$ . Overall conductances are frequently used in heat exchanger design. It is recommended that the total resistance be used in analysis because there is no confusion when it is implemented.

A cylindrical shell  $a \leq r \leq b$  with temperature dependent thermal conductivity, k(T), in the temperature range  $T_2 \leq T \leq T_1$ . Separate the variables T and r, and integrate between appropriate limits:

$$\int_{r=a}^{r=b} \frac{Q \, dr}{2\pi L \, r} = \int_{T=T_1}^{T=T_2} -k_0 (1+\beta T) \, dT$$

where  $k_0$  is the value of k at some reference temperature and  $\beta$  is thermal conductivity temperature coefficient. This is an empirical (experimental) relation. Complete integrations to get

$$\frac{Q}{2\pi L} \ln \frac{b}{a} = k_0 \left( 1 + \frac{\beta}{2} (T_1 + T_2) \right) (T_1 - T_2) = k_{ave} (T_1 - T_2)$$

where  $k_{ave} = k_0 \left(1 + \frac{\beta}{2}(T_1 + T_2)\right)$  is the value of the thermal conductivity at the average temperature of the cylindrical shell  $(T_1 + T_2)/2$ . Thermal resistance of the cylindrical shell is

$$R_{cyl} = \frac{T_1 - T_2}{Q} = \frac{1}{2\pi L \, k_{ave}} \ln \frac{b}{a}$$

A similar analysis can be applied to the plane wall and the spherical shell.

## Lecture 2

Full solution of 1D Laplace equation in cylindrical shell with boundary conditions of the third kind (Robin conditions) at inner and outer boundaries. Found  $T = T(r, a, b, k, h_1, h_2, T_{f_1}, T_{f_2})$  and system heat transfer rate  $Q_{sys}$ . The total resistance of the system consists of three resistances (2 film resistances and 1 solid resistance) in series. Discussion of the physical interpretations of the dimensionless temperature excess and the system heat flow rate.

The full solution can be applied to a plane wall and a spherical shell.

## Lecture 3

Solutions of one-dimensional Poisson equation in plane wall, long solid circular cylinder and solid sphere; all systems are convectively cooled;

see ME 353 Web Site for general equation and general solution with parameter n where n = 0 for plane wall, n = 1 for cylinder, and n = 2 for sphere;

surface temperature rise:  $T_s - T_f = \mathcal{P}b/((n+1)h)$ ;

solid temperature rise:  $T_{max} - T_s = \mathcal{P}b^2/(2(n+1)k)$ ; Biot number for all cases: Bi = hb/(k);

 $\Delta T_{\text{solid}}/\Delta T_{\text{film}} = Bi/2$  for all cases; examples: nuclear fuel element with cladding; ohmic heating in wire with insulation.